

## Facile Determination of Dissolved Species in CO<sub>2</sub>-Amine-H<sub>2</sub>O System by NMR Spectroscopy

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In order to clarify the characteristic behavior of dissolved state of CO<sub>2</sub> in alkanolamine-H<sub>2</sub>O system five different kinds of alkanolamines were examined spectroscopically under the following conditions: 40 °C for 30 min to 120 min. NMR analysis indicated the presence of five chemical species such as carbamate ion, free amine, bicarbonate, carbonate, and protonated amine. Based on proton NMR, distribution of the respective species against molar loading of CO<sub>2</sub> was successfully evaluated.

In the petroleum refining industry, CO<sub>2</sub>-absorption technique by alkanolamine solvent is well known, and the detail has been studied in view of kinetics of gas-liquid reaction.<sup>1-6</sup> This technology is now accepting a lot of attention as a potential method to recover and utilize CO<sub>2</sub> from flue gas. As for the CO<sub>2</sub> recovery by alkanolamine, it is very important to reduce the energy required in this recovery as well as to enhance the CO<sub>2</sub> uptake even at low CO<sub>2</sub> partial pressures because of extremely large quantities of flue gas concerned. In this respect, kinetic study between CO<sub>2</sub> and alkanolamine seems to be the first step to propose more efficient CO<sub>2</sub> absorbents which lead to a lot of reduction in energy consumed.

We have been studying the absorption reaction of CO<sub>2</sub> by using primary, secondary, tertiary, and cyclic amines in the bench scale plant and the pilot plant, finding that secondary amine showed the specific behavior.

In the present study, the dissolved state of CO<sub>2</sub> in aqueous amine solution has been analyzed spectroscopically and the variation of dissolved species with a progress of CO<sub>2</sub> absorption has been examined quantitatively. The following amines are used; monoethanolamine (MEA), 2-(methylamino)ethanol (MAE), 2-(ethylamino)ethanol (EAE), 2-(butylamino)ethanol (BEA), and N-methyl-2,2'-iminodiethanol (MDEA): the samples containing different amount of dissolved CO<sub>2</sub> in 30 wt% aqueous amine (mol of amine: 2.55 - 4.94 mol dm<sup>-3</sup>) are prepared by changing the absorption time and partial pressure of CO<sub>2</sub> from 5 to 100% as are schematically shown in Figure 1. The amount of CO<sub>2</sub> absorbed in amine solution was determined by measuring the CO<sub>2</sub> gas evolved, with NDIR, after the injection of the sample into a reaction tube packed with phosphoric acid-mounted catalyst at 130 °C. <sup>1</sup>H- and <sup>13</sup>C-NMR spectra were obtained using a

JNM-GX270 spectrometer with a capillary sealed TSP [sodium 3-(trimethylsilyl)propanate] as an external standard at 25 °C.

From the plots of molar loading of CO<sub>2</sub> per amine as a function of partial pressure of CO<sub>2</sub>, it is clearly indicated that MAE, EAE, and BEA (secondary amines) have the highest ability to absorb CO<sub>2</sub> while MEA (primary amine) possesses molar loading around 0.5 which shows its less dependence on CO<sub>2</sub> partial pressure and MDEA (tertiary amine), on the other hand, shows the high pressure dependence.

In <sup>1</sup>H and <sup>13</sup>C NMR spectra of the aqueous alkanolamine samples appear the new peaks assigned to carbamate anion, the peak increasing with a progress of CO<sub>2</sub> absorption: much in primary amine, none in tertiary amine and intermediate (between those of primary and tertiary amines) in secondary amine. Beyond some CO<sub>2</sub> loading, however, these peaks decreased gradually, this suggesting the existence of a maximum peak height. The chemical shift of the carbamate formed by the interaction between alkanolamine and CO<sub>2</sub> in aqueous solution is assigned for the first time in this study, the representatives being as follows,

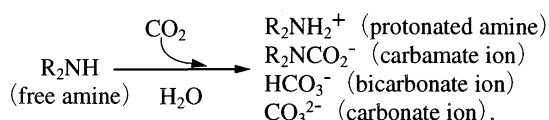
<sup>13</sup>C-NMR δ<sub>N-CO<sub>2</sub></sub> (MEA, sec-Amine) 166-167 (166-167, Amide<sup>7,8</sup>)

δ<sub>C-N</sub> (MEA) 46 (47, Carbamate of DGA<sup>7</sup>)

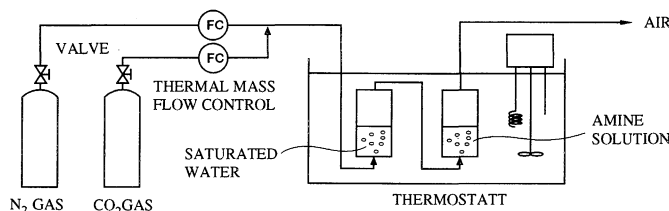
<sup>1</sup>H-NMR δ<sub>N-C-H3</sub> (MAE) 2.87 (2.97, N-methylcarbamate<sup>9</sup>)

δ<sub>N-C-H2</sub> (sec-Amine) 3.32 - 3.35 (3.37, sec-Amine<sup>10</sup>)

Other species derived from the absorption of CO<sub>2</sub> are bicarbonate/carbonate along with free amine/protonated amine, the former being increased continuously and the latter shifted toward the protonated amine with a progress of CO<sub>2</sub> absorption. Therefore, the chemical species in the system with, for example, secondary amine are indicated as follows ;



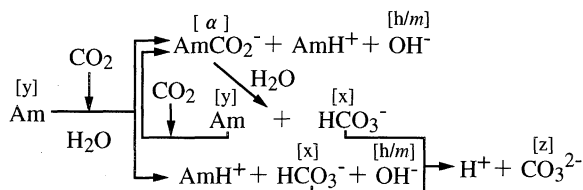
The ratio of the quantities of carbonate ion to those of other amine species can be determined directly by the integration of each peak in the spectra. Quantitative determination of the above five chemical species can be explained using the following scheme by referring to the dissolved species present in the reaction process.



preparation conditions

concentration of amine : 30 wt%  
 amounts of solution : 100 g  
 temperature : 40 ± 0.5 °C  
 flow of gas : 1 dm<sup>3</sup>min<sup>-1</sup>  
 absorption time : 30~120 min

Figure 1. Preparation of the samples containing different amounts of CO<sub>2</sub> in 30 wt% aqueous amine.



The concentration of  $[\text{AmH}^+]$  is sum of  $\alpha$ ,  $x$ ,  $2z$ , and  $h/m$  (on the basis of charge balance, amount of  $[\text{H}^+]$  being negligibly little). If we consider the total amine in the aqueous system  $\{[\text{AmCO}_2^-] + [\text{Am}] + [\text{AmH}^+]\}$  to be 100%, equation (1) is obtained where  $m$  is molar concentration of amine in the system.

$$\alpha + y + \alpha + x + 2z + h/m = 1 \quad (1)$$

From NMR spectra, peak area of carbamate ion and another area of other peaks are assigned a and b, respectively. Equation (2) is obtained.

$$\frac{[\text{carbamate}]}{([\text{free amine}] + [\text{protonated amine}])} = a/b = \frac{[\text{AmCO}_2^-]}{([\text{Am}] + [\text{AmH}^+])} = \alpha/\beta \quad (2)$$

where we employ equation (3).

$$y + \alpha + x + 2z + h/m = \beta \quad (3)$$

Therefore,  $[\text{AmCO}_2^-]: \alpha = \alpha / (\alpha + \beta) = a / (a + b)$  (4)

$$\beta = (1 - \alpha) / (\alpha + \beta) = b / (a + b) \quad (5)$$

From experimental data, we can get  $\text{CO}_2 / \text{total amine}$  ( $\theta$ ), that is,  $\text{CO}_2 / \text{total amine} = ([\text{AmCO}_2^-] + [\text{HCO}_3^-] + [\text{CO}_3^{2-}]) / ([\text{AmCO}_2^-] + [\text{Am}] + [\text{AmH}^+]) = (\alpha + x + z) / (\alpha + \beta) = \theta$ .

From these parameters, we can calculate each concentration of  $[\text{HCO}_3^-]$ ,  $[\text{Am}]$ , and  $[\text{AmH}^+]$  according to the following equations.

$$[\text{HCO}_3^-]: x = \theta \times \beta - (1 - \theta) \times \alpha - z$$

$$[\text{Am}]: y = (1 - \theta) \times \beta - \theta \times \alpha - z - h/m$$

$$[\text{AmH}^+]: \theta + z + h/m$$

where  $z$  and  $h$  are obtained, respectively, by applying the next three equations concerning on the dissociation constant.

$$[\text{Am}][\text{H}^+] / [\text{AmH}^+] = K_p$$

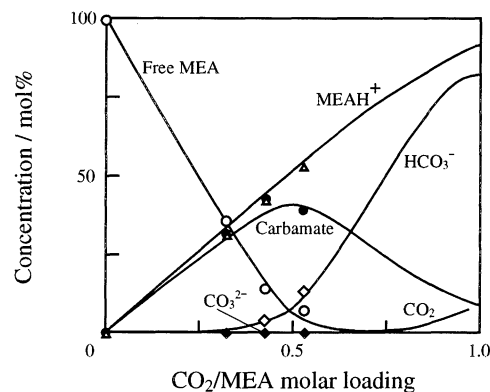
$$[\text{OH}^-][\text{H}^+] = K_w$$

$$[\text{H}^+][\text{CO}_3^{2-}] / [\text{HCO}_3^-] = K_{c2}$$

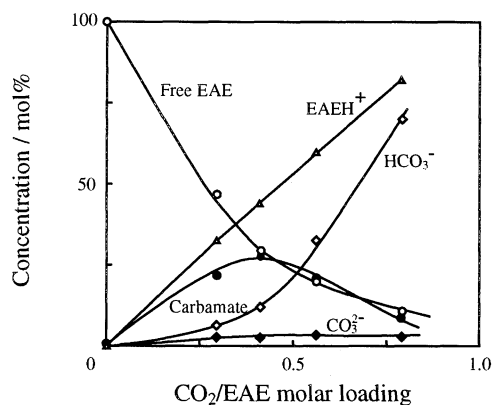
Figure 2 indicates the distribution of five chemical species in the MEA system. The results in this study are plotted with points in the figure and are very similar to that calculated by Austgen *et al.*<sup>11</sup> according to equilibrium of the system where carbamate formation shows maximum at half of molar loading. The proposed method based on NMR measurement, as is shown above, is considered to be the facile method to calculate distribution of chemical species in  $\text{CO}_2$ -Amine- $\text{H}_2\text{O}$  system. Application of this method to three secondary amine systems indicates clearly that the carbamate formation is retarded and bicarbonate forms at lower  $\text{CO}_2$  molar loading than those in MEA system. The results on EAE are shown in Figure 3 as one of the representatives of secondary amines. In the case of MDEA, the results being not shown in the figure, the concentrations of both MDEAH<sup>+</sup> and  $\text{HCO}_3^-$  increase with an increase in  $\text{CO}_2$  molar loading in a similar manner as curves of MEAH<sup>+</sup> and EAEH<sup>+</sup> while free MDEA decreases monotonously because of the lack of carbamate species. The maximum concentration of the carbamate anions examined in this study ranges in the next order;

$$\text{MEA} > \text{MAE} > \text{EAE} \approx \text{BEA} > \text{MDEA} = 0.$$

It is suggested in secondary amine systems that the carbamate may be easily converted by the hydrolysis to both bicarbonate ion and free amine which interacts with another  $\text{CO}_2$  gas, resulting in further increment of absorbed amount. The  $\text{CO}_2$  absorption rate also may be concerned with the carbamate formation since tertiary amine depresses remarkably the absorption rate. The highest ability of secondary amine in  $\text{CO}_2$  absorption may be ascribed for



**Figure 2.** Plots of concentration of chemical species against  $\text{CO}_2/\text{MEA}$  molar loading (points are obtained in this work, lines from the results of D. M. Austgen, *et al.*).



**Figure 3.** Plots of concentration of chemical species against  $\text{CO}_2/\text{EAE}$  molar loading.

the process through the formation of carbamate followed by the easy decomposition to bicarbonate even at low  $\text{CO}_2$  partial pressures because of its moderate carbamate stability.

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## References

- 1 P. V. Danckwerts and K. M. McNeil, *Trans. Instn. Chem. Engrs.*, **45**, 32 (1967).
- 2 G. Astarita, D. W. Savage, and A. Bisio, *Gas Treating with Chemical Solvents*, John Wiley & Sons, New York (1983).
- 3 P. M. M. Blauwhoff, G. F. Versteeg, and W. P. M. Van Swaaij, *Chem. Eng. Sci.*, **39**, 207 (1984).
- 4 E. Sada, H. Kumazawa, and Z. Q. Han, *AIChE J.*, **32**, 347 (1986).
- 5 A. K. Chakraborty, G. Astarita, and K. B. Bischoff, *Chem. Eng. Sci.*, **41**, 997 (1986).
- 6 S. Xu, Y. W. Wang, F. D. Otto, and A. E. Mather, *Chem. Eng. Sci.*, **51**, 841 (1996).
- 7 R. N. Maddox, G. J. Mains, and M. A. Rahman, *Ind. Eng. Chem. Res.*, **26**, 27 (1987).
- 8 G. C. Levy and G. L. Nelson, *J. Am. Chem. Soc.*, **94**, 4897 (1972).
- 9 R. M. Silverstein and G. C. Bassler, *Spectrometric Identification of Organic Compounds*, John Wiley & Sons, New York (1967).
- 10 K. Nukada, O. Yamamoto, T. Suzuki, M. Takeuchi, and M. Ohnishi, *Anal. Chem.*, **35**, 1892 (1963).
- 11 D. M. Austgen, G. T. Rochelle, X. Peng, and C. C. Chen, *Ind. Eng. Chem. Res.*, **28**, 1060 (1989).